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1 Ada	A process for bleaching pulp with ozone, which comprises the steps of
, -	eparing a slurry of cellulosic pulp having a fiber consistency of from 1
to less that	5 weight %;

adding ozone to the cellulosic pulp in a contacting device to create a partial pressure [Pp] of O₃ greater than 1.4 psi and reacting the ozone with the pulp in said contacting device under high shear mixing conditions; and

maintaining the ozone in contact with the pulp for a time sufficient to bleach the pulp.

- 2. The process of claim 1, wherein the partial pressure of ozone applied to the contacting device is sufficient to give at least 0.2 units lower Kappa number as compared to 1.4 psi partial pressure ozone conditions using the same ozone dosage.
- 3. The process of claim 1 for bleaching pulp with ozone wherein the bleached fibers are passed onto a chlorine dioxide bleaching stage.
- 4. The process of claim 1 for bleaching pulp, wherein the cellulosic pulp used to prepare the slurry is obtained from a chlorine dioxide bleaching stage.
- 5. The process of claim 1, wherein the contacting device is a high shear mixer which produces high shear by high rotational speeds across a narrow gap through which the pulp slurry flows.

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6. The process of claim 1 for bleaching pulp, wherein the ozone/cellulosic
pulp is passed into a pressurized retention tube where the ozone reacts with the
lignin in the cellulosic pulp.

- 7. The process of claim 6 for bleaching pulp, wherein the ozone/cellulosic pulp from the retention tube leaves the retention tube through a pressure control valve and is discharged into a separate vessel, where the gas is separated and then passed into an ozone destruct unit before venting to the atmosphere, and the pulp slurry is pumped to a subsequent bleaching stage.
- 8. The process of claim 1 for bleaching pulp, wherein the ozone used in the process is generated on-site from oxygen in a pressurized ozone generator.
- 9. The process of claim 8, in which the ozone generator produces ozone from oxygen at a concentration of from 4 to 20%.
- 10. The process of claim 8, in which the ozone generator produces ozone from oxygen at a concentration of from 10 to 14%.
- 1 11. The process of claim 8, wherein the source of oxygen used for ozone generation is an on site air separation process.
 - 12. The process of claim 11, wherein the air separation process is a vacuum swing absorption process.
 - 13. The process of claim 8 for bleaching pulp with ozone, wherein the ozone gas mixture generated is compressed to a total pressure of from 20-200 psi.

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1	14. The process of claim 8, wherein the ozone gas mixture generated is
2	compressed to a total pressure of from 80 to 150 psi.

- 1 15. The process of claim 1, wherein the partial pressure of ozone created 2 in the contacting device ranges from greater than 1.4 psi up to 43 psi.
- 1 16. The process of claim 1, wherein the partial pressure of ozone created 2 in the contacting device ranges from 9.5 psi to 23 psi.
 - 17. The process of claim 1 for bleaching pulp, wherein the pulp slurry consistency is in the range of from 2 to 4 weight %.
 - 18. The process of claim 1 for bleaching pulp, wherein the ozone is mixed with the cellulosic fibers in the contacting device for a period of time ranging from 0.01 second to 1 minute.
- 1 19. The process of claim 1, wherein the ozone is mixed with the cellulosic fibers in the contacting device for a period of time ranging from 0.04 second to 1 second.
- 1 20. The process of claim 4 for bleaching pulp, wherein the residence time 2 in the retention tube ranges from 1 to 10 minutes.
- 1 21. The process of claim 1 for bleaching pulp, wherein temperature of the pulp slurry entering the mixing with ozone is in the range of from 20 to 80°C.

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- 22. The process of claim 7 for bleaching pulp, wherein the subsequent bleaching stage involves chlorine dioxide as the bleaching agent.
- 1 23. The process of claim 5, wherein a gas meter is present in a conduit to 2 the high shear mixer in order to regulate the flow of gas mixture to the mixer.
 - 24. The process of claim 5, wherein the high shear mixer is connected to an ozone compressor such that the ozone delivered to the high shear mixer contacting device has been first compressed.

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